# **ASIA CLEAN ENERGY FORUM 2025**

Empowering the Future: Clean Energy Innovations, Regional Cooperation and Integration, and Financing Solutions

2-6 June | ADB Headquarters, Manila



# Heehun, Chae / Sunghoon, Park

Senior Researcher HYUNDAI ENGINEERING & CONSTRUCTION



### ASIA CLEAN ENERGY FORUM 2025

Empowering the Future: Clean Energy Innovations, Regional Cooperation and Integration, and Financing Solutions 2-6 June | ADB Headquarters, Manila





# Technology Innovation for Sustainable Energy Transition: Hybrid Carbon Capture and Offshore Storage Solutions

4 June 2025



#### **WHO WE ARE**



#### **ABOUT HYUNDAI E&C**



Hyundai E&C has set out the target of

Net Zero by 2045, reflecting the criteria of SBTi

**VISION : Global Green One Pioneer** 



### **GLOBAL ENERGY TRANSITION FORCAST**



#### Clean Energy Market Growth, Hydrogen Expansion, and the Rising Importance of CCUS

- Global energy demand continues to rise, but fossil fuel demand is expected to peak before 2030.
- In 2022, energy import costs surpassed \$100 trillion,
   highlighting the urgency of energy security and the need for clean energy investment.
- Clean and low-carbon hydrogen production is expected to scale up, with CCUS playing a crucial supporting role in this transition.





[CCU] CO<sub>2</sub> Capture & Liquefaction
 for Blue Hydrogen Production (SMR)

• [CCS] Optimal Storage Design and Facility Conversion Technology for CCS Using Depleted Gas Fields

## **DEMONSTRATION PROJECT IN COMMERCIAL SCALE PLANT**



ADB

#### **CO2 CAPTURE & LIQUIFACTION FOR BLUE HYDROGEN PRODUCTION (SMR)**

- Project Period : '22.05 ~ '25.10 (41month)
- Amount : USD 25.6 Mil (USD 14 Mil, government fund)
- Research target :
  - Commercial-scale demo to optimize CO2 capture in SMR
  - **Capacity** : 81 tCO<sub>2</sub>/d design of commercial scale
  - **Capture** : 90 %1,
  - **CO2 purity** : 95 % ↑
- Main process :
  - Hybrid capture (wet/membrane/VSA)
  - Liquefaction & Storage
- Remark : Commercial operation planned after R&D project

# Challenge in new business utilizing government-Supported R&D Programs



## **DEMONSTRATION PROJECT IN COMMERCIAL SCALE PLANT**





【Status of the Pyeongtaek Hydrogen Production Complex 】

ADB

#### ① Kogastech SMR

- 7t-H $_2$ /d, CO $_2$  capture unit X
- Operation from July '22
  - ► Target of our project

#### ② Kogas SMR

- 15t-H $_2$ /d, CO $_2$  capture unit X
- Under construction from April '25

#### ③ Wonil T&I SMR

- 2t-H<sub>2</sub>/d, CO<sub>2</sub> vspyutr O /liquefaction X
- Operation from May ' 25
  - Target of our project

#### ④ Hyundai consortium CCU

- 81.5t-CO<sub>2</sub>/d capture/liquefaction
- Commissioning from July '25년



## **CONSTRUCTION OF PLANT**

**PROJECT FLOW** 





### **CONSTRUCTION OF PLANT**

#### **TECHNIQUES FOR CO<sub>2</sub> CAPTURE**

	Wet adsorption	Membrane separation	Vacuum swing adsorption
Principle	<ul> <li>Gas-liquid contact</li> <li>physical/chemical absorption</li> </ul>	<ul> <li>Separation using CO<sub>2</sub> permeability through membrane</li> </ul>	<ul> <li>Selective adsorption onto solid adsorbents</li> <li>Regeneration under vacuum</li> </ul>
Advantages	<ul> <li>Most widely used in industry</li> <li>High removal efficiency for large-scale</li> </ul>	<ul> <li>Simple process, easy to expansion</li> <li>Compact and modularized equipment</li> </ul>	<ul><li>Simple design, easy operation</li><li>Highly modular equipment</li></ul>
Disadvantages	<ul><li>Corrosive absorbents</li><li>Handling of circulation is complex</li></ul>	<ul><li>High cost of replacing membranes</li><li>Not suitable for large-scale gases</li></ul>	<ul> <li>Performance may decrease due to catalyst impurities and by-products</li> </ul>
Main element	<ul> <li>Aqueous Absorbent (Amine)</li> </ul>	<ul> <li>Membrane (polymer, ceramic)</li> </ul>	<ul> <li>Solid absorbent (MoF<sup>1)</sup>, zeolite,etc)</li> </ul>
Remark	<ul> <li>Variable cost factor must be considered in feasibility assessment (including pre- and post-treatment, purification, liquefaction, etc.</li> </ul>		



## **CONSTRUCTION OF PLANT**

### PILOT PLANT

OVERALL PLANT	CAPTURE (WET)	CAPTURE (MEMBRANE)	CO2 CAPTURE
<ul> <li>CAPTURE UNIT : WET, MEMBRANE)</li> <li>LIQUEFACTION UNIT</li> <li>UTILITY UNIT : QUENCHER, WWT, etc</li> <li>OPERATION BUILDING</li> </ul>	<ul> <li>CAPACITY : 35 TPD</li> <li>ADSORPTION TOWER</li> <li>STRIPPER</li> <li>ABSORBENT DRUM</li> </ul>	<ul> <li>CAPACITY : 35 TPD</li> <li>MEMBRANE (POLYMER)</li> <li>COMPRESSOR</li> <li>DRYER</li> </ul>	<ul> <li>CAPACITY : 81 TPD</li> <li>COMPRESSOR</li> <li>CHILLER</li> <li>STORAGE TANK</li> </ul>
Liquefaction Wet adsorption Membrane separation	Adsorption tower (39mH)     Regeneration tower (31mH)       BinHi     Control	Gas Compressor	CO2 Storage Tank

## **FUTURE PLAN**



#### **EXPANSION WITH GLOBAL COOPERATION**

- [Similar application] Commercial-scale blue hydrogen / blue ammonia plant project
- [Expansion of target] Expansion to CO2 capture and utilization at high-emission sites (incinerators, landfills, biogas, etc)
- [ Constrains & Suggestions] Boost CCUS fund and carbon market, Relax regulations, Unite certification standard



#### Expansion of target project

• Eco-friendly transformation of incinerator / emission facility



#### Suggestions based on global cooperation

- Ensure economic feasibility by boosting carbon markets and CCUS funds
- Relax rules on international transfer of CCUS and related products, and unify certification standards
- Create CCUS laws to support cooperation between Asian countries



# **CONNECT GLOBAL**,

# **ACHIEVE NET ZERO,**

# **DESIGN OUR FUTURE**





[CCU] CO<sub>2</sub> Capture & Liquefaction
 for Blue Hydrogen Production (SMR)

• [CCS] Optimal Storage Design and Facility Conversion Technology for CCS Using Depleted Gas Fields

# Optimal Storage Design and Facility Conversion Technology for CCS Using ADB Depleted Gas Fields

- Opportunity: Utilization of depleted offshore gas fields
- East Sea Gas Field:

Construction of the East Sea Gas Field production facility began in March 2002. Gas production began in July 2004, and gas production ended on December 31, 2021.

• Donghae CCS Project:

The pre-FEED ordered by the Korea National Oil Corporation (KNOC) in 2023 was carried out.



< Overview of the facility layout for the East Sear Gas Field project, source by KNOC >



< Overview of the facility layout for the depleted East Sea CCS project, source by KNOC >



#### Porthos (Port Of Rotterdam CO<sub>2</sub> Transport Hub and Offshore Storage)

- Location : Rotterdam / North Sea
- CO<sub>2</sub> captured by several companies
- CO<sub>2</sub> transport via pipeline from Rotterdam
- 30km onshore pipeline
- Compressor Station
- 20km offshore pipeline
- Existing offshore platform converted for reuse
- Capacity : 2.5 Mt/y for 15 years, Total 37 Mt
- FID : October 2023
- EPC Start : Early 2024
- Operation : 2026

#### International joint research (Government-Funded)



TNO; Toegepast Natuurwetenschappelijk Onderzoek

Netherlands Organization for Applied Scientific Research



Source : https://www.porthosco2.nl/en/

#### **Composition of Transported Fluid**

 The CO<sub>2</sub> fluid for transportation was designed with CO<sub>2</sub> at a minimum concentration of 95 mol% and H2O at a maximum concentration of 70 ppmv, based on the information collected and analyzed from fluids used in CCS projects worldwide.



#### CO<sub>2</sub> specifications

Component	Mole Base
CO <sub>2</sub>	≥ 95%
H2O	≤ 70 ppm
Sum [H2+N2+Ar+CH4+CO+O2]	≤ 4%
H <sub>2</sub>	≤ 0.75%
N <sub>2</sub>	≤ 2.4%
Ar	≤ 0.4%
CH4	≤ 1%
CO	≤ 750 ppm
O2	≤ 40 ppm
Total sulfur-contained compounds (COS, DMS, H <sub>2</sub> S, SOx, Mercaptan)	≤ 20 ppm
	Of which $H_2S \leq 5$ ppm
Total NOx	≤ 5 ppm
Total aliphatic hydrocarbons (C2 to C10) <sup>i</sup>	≤ 1200 ppm
Total aromatic hydrocarbons (C6 to C10, incl. BTEX) <sup>i</sup>	≤ 0.1 ppm
Total volatile organic compounds <sup>ii</sup> (excl. methane, total aliphatic HC	≤ 10 ppm
(C2 to C10), methanol, ethanol, and aldehydes)	
Total aldehyde compounds	≤ 10 ppm
Ethanol	≤ 20 ppm
Methanol	≤ 620 ppm
Hydrogen cyanide (HCN)	≤ 2 ppm
Total amine compounds	≤ 1 ppm
Total glycol compounds	Follow dew point specification
Ammonia (NH3)	≤ 3 ppm
Total carboxylic acid and amide compounds	≤ 1 ppm
Total phosphorus-contained compounds	≤ 1 ppm
Toxic compounds <sup>iii</sup>	
Dew point limit value measurement (for all liquids, i.e. for complete	< -10 °C (at 20 bara)
CO <sub>2</sub> composition)	
Note i: Specification values are molecular based Note ii: VOC definition according to Dutch policy Note iii: Toxic compounds: although CO <sub>2</sub> and other gases like i.e. H <sub>2</sub> and N <sub>2</sub> can form a risk of asphyxiat within the stream which impose a risk on personal safety to be taken into account in Porthos HSE policy	ion, Porthos would like to know other components

< the CO<sub>2</sub> specifications for storage in the Netherlands PORTHOS CCS project, Source : <u>https://www.porthosco2.nl/en/</u> >





#### **Capacity Design**

- The conditions of CO<sub>2</sub> entering the CCS onshore compression facility and the conditions of CO<sub>2</sub> being transported through the subsea pipeline after compression are as follows and were used as key boundary conditions for this study.
- The average  $CO_2$  output through the compression facility is 2.5 Mtons of  $CO_2$  per year.
- Considering an annual operation of 8,000 hours and a margin rate of 10%, the maximum hourly output is 343.8 tons of CO<sub>2</sub> per hour.

Location	Boundary Conditions
Onshore Plant Inlet	30°C, 35 barg, 343.8 ton-CO <sub>2</sub> /h
Onshore Plant Outlet	80°C, 130 barg, 343.8 ton-CO <sub>2</sub> /h
Offshara Dlatform Inlat	80°C, 130 barg, 343.8 ton-CO <sub>2</sub> /h (temperature and pressure drops in
	the offshore pipeline are ignored, using maximum values for this study)
Offshore Platform Outlet	343.8 ton-CO <sub>2</sub> /h

[Table - Boundary Conditions]



#### **Onshore Equipment List**

- The onshore facilities are the core process systems for CO<sub>2</sub> transport, designed to discharge CO<sub>2</sub> at 150 barg and 80°C through two-stage compression and cooling configured in three trains.
- Impurities are separated through an inlet filter separator, and the required temperature and pressure are adjusted through suction and discharge drums and CO<sub>2</sub> coolers.
- Other items are assumed to consist of generally necessary equipment.

Inlet filter separator		
1st Stage Compressor Suction Drum		
2nd Stage Compressor Suction Drum		
2nd Stage Compressor discharge drum		
1st Stage CO2 Compressor		
2nd Stage CO2 Compressor		
Motor for CO2 compressor		
1st Stage CO2 Cooler		
2nd Stage CO2 Cooler		
Metering unit		
Pig Launcher		



#### **Offshore Equipment List**

- The offshore platform is designed to inject CO<sub>2</sub> into depleted gas fields or saline aquifers, with compressed CO<sub>2</sub> transported from the onshore facility via a 16-inch, 21 km subsea pipeline.
- It includes choke and safety valves, control systems, a manifold connected to four risers for injection, and an umbilical for subsea operations.
- A pig receiver is also installed for pipeline maintenance.
- Additionally, space is allocated for future installations of booster pumps, an electric heater, and control systems for potential subsea operations.





#### **CCS** demonstration project using the **Donghae-1** depleted gas reservoirs

- Location : Ulsan / East Sea
- CO<sub>2</sub> captured by several companies
- CO<sub>2</sub> transport via pipeline from Ulsan
- Onshore Hub Terminal
- Approx. 60km offshore pipeline
- Existing offshore platform converted for reuse
- Reuse of production wells
- Capacity : 1.2 Mtpa for 10 years
- Expected FID : 3Q 2025
- Expected EPC Start : Early 2026
- Expected Operation : After 2028





#### **Composition of Transported Fluid**

The CO<sub>2</sub> stored at the East Sea Gas Field comprises emissions from Steam Methane Reforming (SMR) ٠ processes for hydrogen production and flue gases from nearby thermal power plants. As shown in below Table, the stored  $CO_2$  has a purity level of 99.26%.



[Table – Specification of CO<sub>2</sub> Fluid ]

Component	Mol (%)
CO <sub>2</sub>	99.26
CO	0.01
H <sub>2</sub>	0.6
$CH_4$	0.12
H <sub>2</sub> O	0.01



#### **Capacity Design**

- The Korean government is preparing a 1.2 MTPA CCS project
- On the platform, the CO<sub>2</sub> passes through choke valves that regulate flow to three wells
- Well 2P, the depleted gas well with the lowest pressure. Production continued until this well reached a very low pressure of 33 bar, a significant decrease from the initial production pressure of 248 bar.

[Table – Reservoir condition of East S	Sea Gas Field (Well 2P)]	C-PT-SUBSEAD/PELINE Offshore Platform ~ Wellhead
Contents	Value	$\rightarrow 2km$ $C-GT-WELL-1P$ $PD$ $Wellhead ~ Bottomhole$ $\rightarrow 2.7km$
Pressure (Depleted, After production)	33 bar	2XXM-RPELINE-1P         Well-1P         E-3 X         BH-1P           2XXM-RPELINE-1P         Well-1P         E-3 X         BH-1P           C-GT-Well-2P         Well-1P         Reservoire-1P           WH-2P         WH-2P         WH-2P         WH-2P
Pressure (Initial, Before production)	248 bar	$\begin{array}{c c c c c c c c c c c c c c c c c c c $
Temperature	104 ℃	
Depth	2600 ~ 2800 m	

[OLGA simulation model for 1.2 mil ton/yr  $CO_2$  injection ]



#### **Onshore Equipment List**

- The facility is capable of processing 1.2 MTPA of CO<sub>2</sub>, handling 1.1 MTPA of gaseous CO<sub>2</sub> and 0.1MTPA of liquid CO<sub>2</sub> annually.
- It consists of CO<sub>2</sub> Inlet, Dehydration, Compression, Liquefaction, Storage, and Export infrastructures.

	Inlet Separator	
CO₂ Inlet	CO <sub>2</sub> Gas Metering Package	
	Pig Receiver	
CO₂ Dehydration	CO <sub>2</sub> Dryer	
	Regeneration Gas Heater	
	Regeneration Gas Cooler	
	Regeneration Gas K.O Drum	

	CO <sub>2</sub> Booster Compressor Suction Drum	
	CO <sub>2</sub> Booster Compressor	
	CO <sub>2</sub> Booster Compressor Inter Cooler	
	Interstage KO Drum	
CO Comprossion	CO <sub>2</sub> Booster Compressor After Cooler	
$CO_2$ Compression	After-stage KO Drum	
Liquefaction	Chiller	
	Refrigerant Compressor	
	Refrigerant Condenser	
	Refrigerant Receiver	
	Compressor Suction KO Drum	
	LCO₂ Storage Tank	
	LCO <sub>2</sub> Unloading Pump	
	LCO <sub>2</sub> Truck Weighing Gauge	
LCO <sub>2</sub> Storage	LCO₂ Export Pump	
Export	LCO <sub>2</sub> Metering Package	
	Pig Launcher	
	Chemical Injection Package	



#### **Offshore Equipment List**

- To be designed to inject LCO<sub>2</sub>, transported via pipeline from the CO<sub>2</sub> terminal to the offshore platform, into reservoirs through injection wells using LCO<sub>2</sub> injection pumps.
- Pigging operation facilities for connecting LCO<sub>2</sub> transported from the onshore CO<sub>2</sub> terminal to the injection system on the offshore platform, and for cleaning and maintaining the subsea pipeline.
- Equipment for transferring liquefied CO<sub>2</sub>, which conditions the fluid to the required temperature and pressure for final injection into the subsea reservoir and facilitates LCO<sub>2</sub> injection.

Inlet	CO <sub>2</sub> Import Pig Receiver
	CO <sub>2</sub> Injection Filters
	CO <sub>2</sub> Buffer Vessel
Injection	CO <sub>2</sub> Buffer Vessel Pressure Build-up Unit
	CO <sub>2</sub> Injection Pump
	CO <sub>2</sub> Metering Skid



## **Conclusion : Comparison**

#### Summary

Contents	Porthos	Donghae
Stage	EPC	FID
CO <sub>2</sub> Phase	Gas	Liquid
Onshore Facilities	Compression	Dehydration & Liquefaction
Offshore Platform Power Source	Green	From Shore
Reuse Existing Facilities	Offshore Platform, Injection Well	Offshore Platform, Injection Well, Subsea Pipeline
Subsea pipeline	New : CCS Injection Existing : Gas production	Existing : CCS Injection